XP-002278112

AN - 1985-124697 [21]
AP - JP19830168009 19830912
CPY - MITN
DC - E17
DR - 0270-S 0966-S
FS - CPI
IC - B01J27/16 ; B01J29/06 ; B01J31/08 ; C07C41/06 ; C07C43/04
MC - E10-H01 N05-E
M3 - [01] H5 H581 H8 M210 M211 M214 M233 M272 M282 M320 M416 M620 M720 M903 N213 N262 N309 N342 N441 N470 N513 N522
- [02] M423 M730 M903 Q421
PA - (MITN ) MITSUBISHI GAS CHEM CO INC
PN - JP60058932 A 19850405 DW198521 006pp
PR - JP19830168009 19830912
XA - C1985-054056
XIC - B01J-027/16 ; B01J-029/06 ; B01J-031/08 ; C07C-041/06 ; C07C-043/04
AB - J60058932 Methyl t.-butyl ether (I) is prepd. by passing a mixt. of isobutylene (II) and methanol (III) through an adiabatic reactor to give a reaction mixt. of (I), (II) and (III), leading to a reactive distn. tower and isolating (I) after reaction.
- Spent BB fraction contg. 45% (II) is used as raw material for (II). Solid catalyst Amberlite 200C (RTM) pre-swollen with (III).
- ADVANTAGE - (I) is prepd. continuously from (II) and (III). Conversion of (II) and reaction rate to (I) are excellent using a simple and compact reactor while economising with energy.
- In an example, 1.1 mol. eq. methanol to isobutylene in spent BB fraction was fed into an adiabatic reactor at 26 kg/hr under pressure. Temp. around catalyst inlet of adiabatic reactor was 55 deg.C (pressure of 8 kg/cm2G), and that of catalyst exit 81 deg.C. Pressure at summit of reactive distillation tower was 7.5 kg/cm2G. Reaction mixt. was supplied from adiabatic reactor to reactive distn. tower. Conversion ratio of (II) was 89% and that in the tower 93%. Total conversion ratio was 99%.(0/1)
IW - METHYL BUTYL ETHER PREPARATION PASS MIXTURE ISOBUTYLENE METHANOL THROUGH ADIABATIC REACTOR REACT DISTIL TOWER
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NC - 001
OPD - 1983-09-12
ORD - 1985-04-05
PAW - (MITN ) MITSUBISHI GAS CHEM CO INC
TI - Methyl t-butyl ether prepn. - by passing mixt. of isobutylene and methanol through adiabatic reactor and then to reacting distn. tower